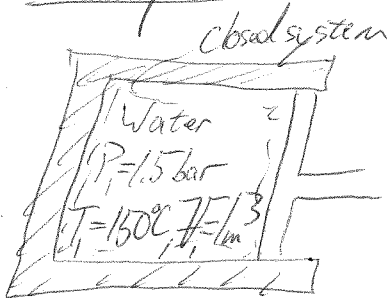


Closed System Energy Balances:

- Last week we covered properties ^{models} of fluids, the week before we discussed ^{Energy} systems & balances
- Today we start putting everything together: Balances, Energy, & fluid properties

Example: Water is compressed in a series of steps:



1) First it is compressed @ constant temperature until liquid water droplets begin to form. This process is maintained @ constant temperature by heat transfer to the surroundings.

2 → 3) The piston is pushed in further until $V_3 = 0.05 \text{ m}^3$ again @ constant temperature

Find: the heat transfer from 2 → 3 to maintain the constant temperature.

★ How do we begin? Let's establish some general steps for problem solving.

Step 1: Draw & Define the system.

Step 2: List assumptions about the problem

- 1) Pure water (real fluid model), 2) sealed piston/closed system, 3) rigid cylinder,
- 4) no ΔPE , ΔKE , or ΔME , 5) process is incremental

Step 3: Apply Balances & Simplify (if needed)

Mass Balance: $M_{in} + M_{produced} = M_{out} + M_{destroyed} + \Delta M_{stored} \Rightarrow \Delta M_{stored} = M_2 - M_1 = 0$

$M_2 = M_1$

Energy Balance: $E_{in} + E_{produced} = E_{out} + E_{destroyed} + \Delta E_{stored} \Rightarrow$

$\Rightarrow \underset{0(5)}{Q_{in}} + \underset{0(5)}{W_{in}} = \underset{0(4)}{Q_{out}} + \underset{0(4)}{W_{out}} + \Delta \underset{0(4)}{U} + \Delta \underset{0(4)}{P} + \Delta \underset{0(4)}{K} + \Delta \underset{0(4)}{E} \Rightarrow$

$\Rightarrow W_{in} = Q_{out} + \Delta U \Rightarrow m(u_2 - u_1)$

$\hookrightarrow P_{Twork} \Rightarrow P_{Twork} = - \int_{T_2}^{T_3} P dT$

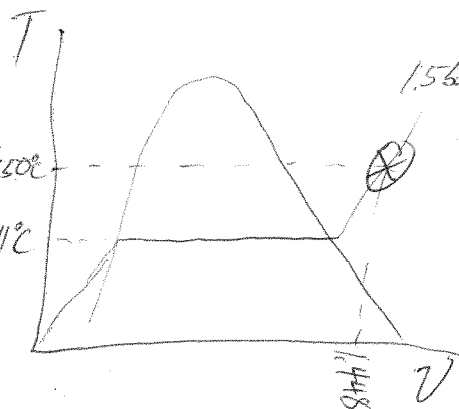
$\rightarrow$ P_{Twork} in compression must be negative because

$T_3 < T_2$ & work is going into the system. So we know that the work term must be ^{positive} & this sign is needed.

$\rightarrow - \int_{T_2}^{T_3} P dT = Q_{out} + m(u_3 - u_2)$

this is about as simplified as we can make it.

Step 4: Apply fluid model, Draw diagram, & fix the states



State 1: $P_1 = 1.5 \text{ bar}$, $T_1 = 150^\circ\text{C}$, $T_{sat} = 111.3^\circ\text{C}$

Vapor Table A-5: $T_{sat} = 111.3^\circ\text{C}$ so we must be in the superheated vapor region

Goto Table A-6 to find v & u

@ 100 kPa & 150°C $v = 1.9367 \text{ m}^3/\text{kg}$, $u = 2582.9 \text{ kJ/kg}$

@ 200 kPa & 150°C $v = 0.95986$, $u = 2577.1 \text{ kJ/kg}$

We need to Interpolate!

$\frac{P - P_{low}}{P_{high} - P_{low}} = \frac{v - v_{low}}{v_{high} - v_{low}} \Rightarrow \frac{150 - 100}{200 - 100} = \frac{v - 1.9367}{0.95986 - 1.9367} \Rightarrow v_1 = 1.448 \text{ m}^3/\text{kg}$

$\frac{P - P_{low}}{P_{high} - P_{low}} = \frac{u - u_{low}}{u_{high} - u_{low}} \Rightarrow \frac{150 - 100}{200 - 100} = \frac{u - 2582.9}{2577.1 - 2582.9} \Rightarrow u_1 = 2580 \text{ kJ/kg}$

ME301/201263

We can find the mass of water in the tank now:

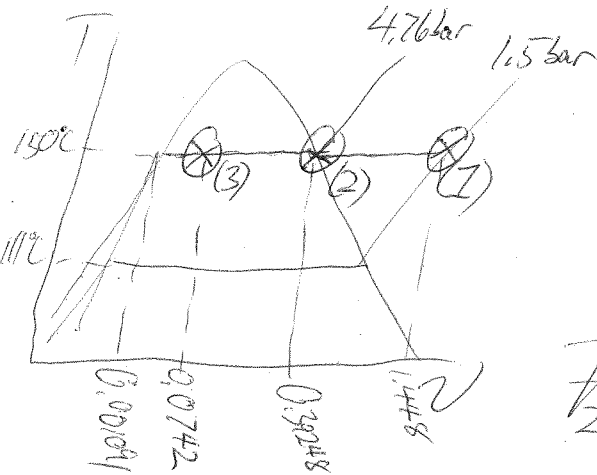
$$M = \frac{F_1}{v_1} = \frac{1 \text{ m}^3}{1.448 \text{ m}^3} \Rightarrow M = 0.690 \text{ kg}$$

Now find state 2: Compressed @ constant T until droplets form: $x_2 = 1.0$

$$T_2 = 150^\circ\text{C}$$

Which table? Saturated water A-4 @ $T_2 = 150^\circ\text{C}$

We see that $P_2 = 4.76 \text{ bar}$ $v_{g,2} = 0.39248 \text{ m}^3/\text{kg}$
 $u_{g,2} = 2559.1 \text{ kJ/kg}$



$$F_2 = ? = M v_{g,2} = 0.690 \text{ kg} (0.39248 \text{ m}^3/\text{kg}) \Rightarrow F_2 = 0.271 \text{ m}^3$$

Now find state 3: Compressed @ constant T until $F_3 = 0.05 \text{ m}^3$, $T_3 = 150^\circ\text{C}$

What can we find? we know that $v_{f,2} = 0.001091 \text{ m}^3/\text{kg}$ are we above this?

$$v_3 = \frac{F_3}{M} = \frac{0.05 \text{ m}^3}{0.690 \text{ kg}} \Rightarrow v_3 = 0.0742 \text{ m}^3/\text{kg}$$

Yes we're in the vapor dome

But how to find u_3 ? $\rightarrow$ find the quality: $x_3 = \frac{v_3 - v_f}{v_g - v_f} = \frac{0.0742 - 0.001091}{0.39248 - 0.001091} \Rightarrow x_3 = 0.187$

$$x_3 = \frac{u_3 - u_f}{u_g - u_f} \Rightarrow u_3 = u_f + x(u_g - u_f) \Rightarrow u_3 = 631.66 + 0.187(1927.4) \Rightarrow u_3 = 992.08 \text{ kJ/kg}$$

Volume of just the liquid? $x = 1 - \frac{M_f}{M} \Rightarrow M_f = (1 - x)M = (1 - 0.187)0.690 \text{ kg}$
 $M_f = 0.561 \text{ kg}$

$$F_{liq} = M_f v_f = 0.561 \text{ kg} / 0.001091 \text{ m}^3 \Rightarrow F_{liq} = 0.000612 \text{ m}^3$$

6.4 ME301 Sp 2012

Step 5: Now solve balance: ~~state~~ $-\int_{V_2}^{V_3} P dV = Q_{out} + m(u_3 - u_2)$

State 2 $\rightarrow$ 3 process occurs @ constant pressure

$$-P(V_3 - V_2) = Q_{out} + m(u_3 - u_2) \Rightarrow Q_{out} = -P(V_3 - V_2) + m(u_2 - u_3)$$

$$Q_{out} = 476,000 \text{ Pa} (0.27 \text{ m}^3 - 0.05 \text{ m}^3) + 0.09 \text{ kg} (2559,100 \frac{\text{J}}{\text{kg}} - 997,080 \frac{\text{J}}{\text{kg}})$$

$$Q_{out} = 1,186,000 \text{ J} \Rightarrow Q_{out} = 1.186 \text{ MJ}$$

$\rightarrow$ Heat left the system as the sign is still positive,
makes sense with engineering judgement