

Properties of Pure Fluids: Incompressible & Ideal

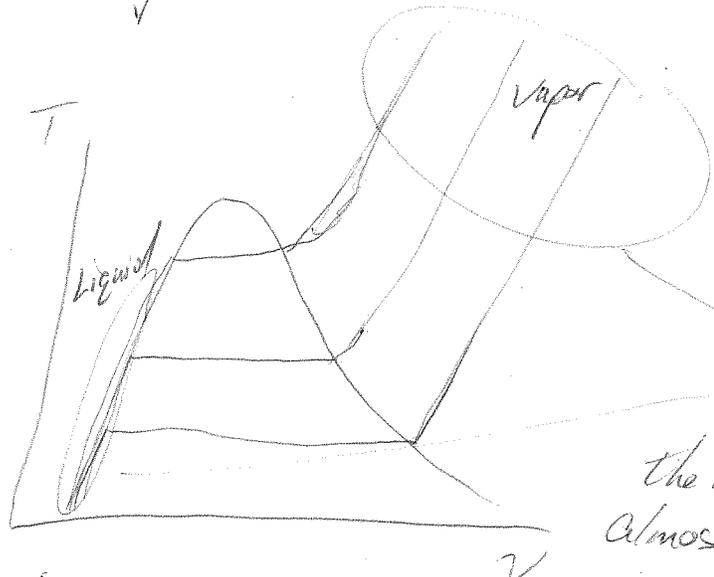
ME 301 Sp 2012 5.1

Last time you were given states of a fluid & had to look up property information using tables in the back of your book & sketch a T-v plot. Let's do your homework with software like EES.

$T_1 = 200^\circ\text{C}$, $x_1 = 0$, $P_2 = 0.5 \text{ bar}$, $x_2 = 1$, $P_3 = 0.75 \text{ bar}$, $v_3 = 0.1 \text{ m}^3/\text{kg}$, $T_4 = 400^\circ\text{C}$, $u_4 = 2850 \text{ kJ/kg}$
 $T_5 = 100^\circ\text{C}$, $P_5 = 100 \text{ bar}$

Show with Arrays & make a property plot in EES.

- How are these tables & property plots made? → show fluid into for water
- Some EOS have over 50 terms!!! In some situations it can become computationally taxing to use this complicated equation on a simple problem.
- Let's look at the plot we just made to see if there are any simplifications we can make:



In these two regions the isobars become almost straight!

→ Early Scientists & engineers noticed relatively simple areas of fluid EOS.

→ very little change in volume for a huge change in pressure.

Incompressible Substance



Parts
 for Incompressible Substance model for Solids & liquids far from vapor dome:

$$1) v = \text{constant} = \rho$$

2) internal energy \rightarrow before it was tabulated or from software, now we can express it as only a function of temperature.

\rightarrow We defined internal energy as the energy stored by molecules.

\rightarrow What property is probably closely related to this? \rightarrow heat capacity

\rightarrow The heat capacity of an incompressible substance is defined as

difference between C_p & C_v is small, so just use C

$$C = \frac{du}{dT} \Rightarrow du = C dT \Rightarrow \int_{u_1}^{u_2} du = \int_{T_1}^{T_2} C dT \Rightarrow u_2 - u_1 = \int_{T_1}^{T_2} C dT$$

$\rightarrow C$ varies with temperature!! However it is usually a small change so in this class we'll ^{generally} assume it's constant.

For incompressible substance: $u_2 - u_1 = C(T_2 - T_1)$



\rightarrow Far away from the vapor dome in the gas region the isobars are almost linear: $Pv = RT$

Ideal Gas

These lines are linear because the molecules are not interacting strongly etc. with one another.

Parts to ~~the~~ Ideal Gas model for gases far away from vapor dome:

1) Ideal Gas Law: $Pv = RT$ $\rightarrow R = \frac{R_{universal}}{\text{molecular weight}}$ \leftarrow Gas Constant \leftarrow Values tabulated in Appendix A-2 of book

2) $u = u(T) \rightarrow$ internal energy is only a function of temperature
 \rightarrow here, unlike the incompressible substance model, differences are computed using the specific heat capacity @ constant volume: C_v

$C_v = \left(\frac{\partial u}{\partial T}\right)_v \Rightarrow C_v = \frac{du}{dT} \Rightarrow du = C_v dT \Rightarrow \int_{T_1}^{T_2} du = \int_{T_1}^{T_2} C_v dT \Rightarrow$

$\Rightarrow u_2 - u_1 = \int_{T_1}^{T_2} C_v dT$ \leftarrow C_v is a function of temperature
 Sometimes we will assume C_v is constant over small ΔT
 then $u_2 - u_1 = C_v(T_2 - T_1)$ for ideal gas

If C_v is not constant we have 3 options:

- 1) Solve Integral of nasty function We want to do this
- 2) Ideal Gas tables in book slow
- 3) Ideal gas function in software

Example of different methods in EES: $CO_2 @ T_2 = 200^\circ C, P_2 = \text{atm}, T_1 = 100^\circ C, P_1 = \text{atm}$

1) real fluid: $\Delta u_{real} = \text{intenergy}(\text{Carbon dioxide}, T=T_2, P=P_2) - \text{intenergy}(\text{Carbon dioxide}, T=T_1, P=P_1)$

2) ideal fluid: $\Delta u_{ideal} = \text{intenergy}(CO_2, T=T_2) - \text{intenergy}(CO_2, T=T_1)$

No function for this in EES

Chemical symbols in EES are only used for ideal gas functions

3) ideal constant C_v : $\Delta u_{const} = C_v(T_2 - T_1) \leftarrow C_v = 706 \text{ J/kg}\cdot K \leftarrow 0.3\% \text{ error} \leftarrow 8.3\% \text{ error}$

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Important Notes for ~~Class~~ Selecting a Fluid Model

if you switch you
may destroy energy.
↓

- 1) Pick a model & stick with it for the problem → be consistent
- 2) Don't worry about the absolute value of u ! the values are way different
 $u_2 = \text{intenergy}(\text{carbon dioxide}, T=T_2, P=P_2)$, $u_{2, \text{ideal}} = \text{intenergy}(\text{CO}_2, T=T_2)$
Why? How? $u=0$ is defined relative to a reference state
it doesn't matter because you will always compute Δu 's.
- 3) I will generally tell you in problems ~~when~~ if you can use incompressible substance or ideal gas.
- 4) You will have to use your engineering judgment to pick models